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## Journal of Liquid Chromatography & Related Technologies

Publication details, including instructions for authors and subscription information:

<http://www.informaworld.com/smpp/title~content=t713597273>

### Studies on Environmental Pollutants: Selective Separation and Recovery of Pb(II) on Ferric Phosphate Columns

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**To cite this Article** Thind, Pritam Singh and Singh, Harbans(1981) 'Studies on Environmental Pollutants: Selective Separation and Recovery of Pb(II) on Ferric Phosphate Columns', *Journal of Liquid Chromatography & Related Technologies*, 4: 8, 1473 – 1485

**To link to this Article:** DOI: 10.1080/01483918108059622

**URL:** <http://dx.doi.org/10.1080/01483918108059622>

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STUDIES ON ENVIRONMENTAL POLLUTANTS: SELECTIVE SEPARATION  
AND RECOVERY OF Pb(II) ON FERRIC PHOSPHATE COLUMNS

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ABSTRACT

A new method is described for the recovery and selective separation of Pb(II). The following mixtures have been separated: Hg(II)-Pb(II), ZrO(II)-Pb(II), Cd(II)-Pb(II), Cu(II)-Pb(II), Mn(II)-Pb(II), Zn(II)-Pb(II), Sr(II)-Pb(II) and Ni(II)-Pb(II), on ferric phosphate columns. Cu(II), Cd(II), Ni(II), Hg(II), Mn(II), Zn(II), Sr(II) and ZrO(II) were eluted with 0.01M-NH<sub>4</sub>NO<sub>3</sub> and Pb(II) with a mixture of 0.1M-HNO<sub>3</sub> + 1.0M-NH<sub>4</sub>NO<sub>3</sub> solution. Proposed studies can be applied to pollution analysis and alloy analysis.

INTRODUCTION

Lead poisoning has long been known and has been exhaustively studied. Although fatal cases of plumbism are now relatively rare, lead and its compounds still constituted one of the most important industrial hazards. Serious lead intoxication is most frequently encountered in persons who have inhaled the vapours, fumes or dust of lead and lead containing compounds. For example, the process of sanding and spraying lead paints are extremely

hazardous with adequate protection. The allowable limits of lead in potable water (1) and air (2) as fixed by U.S. Public Health Service is 0.2-2  $\mu\text{g}/\text{l}$  and 0.15  $\text{mg}/\text{cubic meter of air}$  respectively. The recovery and selective separation of lead in water and in other various biological samples is necessary with the view point of pollution studies. In continuation of our work on analytical applications of ion exchange materials (3-5), the present communication extends our studies to the application of ferric phosphate, an inorganic ion exchanger, for the selective separation and recovery of lead.

### EXPERIMENTAL

#### Apparatus:

A glass column (i.d. 1.3cm) was used for column operation. 1.0g. of ferric phosphate ( $\text{H}^+$ -form) was taken in the column and flow rate was initially maintained at 1.5ml/minute.

For pH measurements an ELICO pH meter model LI-10 was used.

#### Reagents and Chemicals:

Ferric nitrate (BDH) and ammonium dihydrogen phosphate (BDH) were used. All other chemicals were of analytical grade.

#### Synthesis of Ferric phosphate:

Ferric phosphate was prepared by adding 0.1M aqueous solution of ammonium dihydrogen phosphate to 0.1M-ferric nitrate solution as described earlier(4). The dried product was converted into the  $\text{H}^+$ -form by treating with 0.1M nitric acid for 24h with occasional shaking and intermittent changing of the acid. The product thus formed was dried at 40°C in a temperature controlled oven.

Distribution Studies:

The distribution studies were carried out for 19 metal ions by batch process in the usual manner (4) after attaining equilibrium by shaking the metal ion solution with exchanger beads for 6 hours at room temperature ( $30^{\pm}1^{\circ}\text{C}$ ). The distribution coefficients ( $K_d$ ) for metal ions were calculated by using the following expression:

$$K_d = \frac{I-F}{F} \times \frac{20}{0.2}$$

where I is the volume of EDTA consumed by the original solution and F is the volume of EDTA consumed after equilibrium. The total volume of solution was 20 ml and the amount of exchanger used was 0.2g.

Elution behaviour:

From preliminary elution studies of Pb(II), Cu(II), Ni(II), Cd(II), Hg(II), Zn(II), Mn(II), Sr(II) and Zr(II), it is observed that Pb(II) remains strongly adsorbed on ferric phosphate ( $\text{H}^+$ -form) bed in 0.01M- $\text{NH}_4\text{NO}_3$  whereas Cu(II), Ni(II), Cd(II), Hg(II), Zn(II), Mn(II), Sr(II) and Zr(II) percolate through the exchanger bed and quantitatively collected in the effluent. The flow rate is kept at 1.5ml/minute. After removal of Cu(II), Ni(II), Cd(II), Hg(II), Zn(II), Mn(II), Sr(II), and Zr(II), Pb(II) can be eluted quantitatively with a mixture of 0.1M- $\text{HNO}_3$ +1.0M- $\text{NH}_4\text{NO}_3$  (1:1) solution.

Procedure:

The ion exchanger column ( $\text{H}^+$ -form) was washed with demineralized water before passing the test solution. A known volume of test solution (or synthetic mixture) was taken accurately and was recycled thrice through the exchanger bed at the flow rate of 1.5ml/minute. The column was then washed with 0.01M- $\text{NH}_4\text{NO}_3$ . Cu(II), Ni(II), Cd(II), Hg(II), Zn(II), Mn(II), Sr(II) and Zr(II) were percolated out with the effluent and washing liquid, the adsorbed Pb(II) was then eluted quantitatively with a mixture of 0.1M- $\text{HNO}_3$ +1.0M- $\text{NH}_4\text{NO}_3$  (1:1) solution.

### RESULTS AND DISCUSSION

The distribution coefficients ( $K_d$ ) of the cations are reported in TABLE-I. It is obvious from the results that the  $K_d$  values of Cu(II), Ni(II), Cd(II), Hg(II), Zn(II), Pb(II), Sr(II) and ZrO(II) are approximately ten times less than Pb(II) hence Pb(II) can be separated from these metals.

#### Recovery of Pb(II):

TABLE-II shows the successful recoveries of Pb(II) from solutions containing Cu(II), Ni(II), Cd(II), Hg(II), Zn(II), In(II), Sr(II) and ZrO(II). In the presence of five fold excess of these metal ions, all of them could be eluted with 0.01N-NH<sub>4</sub>NO<sub>3</sub> except Pb(II). The retained Pb(II). The retained Pb(II) was easily eluted with a mixture of 0.1N-HNO<sub>3</sub> + 1.0N-NH<sub>4</sub>NO<sub>3</sub> (1:1) solution. This shows the importance of ferric phosphate in the recovery of Pb(II).

#### Column Separation:

Unlike Pb(II) which was retained by the exchanger, Cu(II), Ni(II), Cd(II), Hg(II), Zn(II), Pb(II), In(II), Sr(II) and ZrO(II) passed out uncorbed. Quantitative separations of these metal ions from Pb(II) have been successfully achieved. TABLE-III shows a list of separations successfully achieved on a column of ferric phosphate. The order and the eluents are presented in Figures 1-8.

The minimum number of theoretical plates(N) necessary for separation as tabulated in TABLE-III were calculated using equation

$$N \geq 2\pi \left[ \frac{\frac{K_{d,Pb} + a}{K_{d,M} + a} + 1}{\frac{K_{d,Pb} + a}{K_{d,M} + a} - 1} \right]^2$$

where  $K_{d,Pb}$  and  $K_{d,M}$  are distribution coefficients of lead

TABLE-I  
 Distribution coefficients of Metal Ions on Ferric Phosphate in Water (pH = 5-6)

Metal ions	$K_d$	Metal ions	$K_d$	Metal ions	$K_d$
Ni(II)	18.2	Ca(II)	14.3	Cd(II)	12.5
Zn(II)	11.3	Sr(II)	9.0	Hg(II)	75.0
Mn(II)	9.8	Ba(II)	20.8	Ni(III)	46.4
Ni(II)	15.5	Cu(II)	6.6	Yb(II)	52.0
Co(II)	53.0	Pb(II)	130.0	Al(III)	100.0
ZrC(II)	9.8	La(III)	52.2	Cr(III)	54.6
Th(IV)	T.A.				

Note: T.A. = Totally Adsorbed.

TABLE-II  
 Recovery of Pb(II) from Solutions Containing 5,000 $\mu$ g Each  
 of Cu(II), Ni(II), Co(II), Hg(II), Zn(II), Mn(II), Sr(II)  
 and ZrC(II)

Recovery of Eluents	Volume of eluent (ml)	Amount of Pb(II) loaded ( $\mu$ g)	Recovered ( $\mu$ g)	Error%
Pb(II) from Impurities-0.01M-NH <sub>4</sub> NO <sub>3</sub>	50	-	-	-
Pb(II) from Impurities-0.1M-HNO <sub>3</sub> +1.0M-NH <sub>4</sub> NO <sub>3</sub>	10	1,000	1,000	0.0
Pb(II) from Impurities-0.01M-NH <sub>4</sub> NO <sub>3</sub>	60	-	-	-
Pb(II) -0.1M-HNO <sub>3</sub> +1.0M-NH <sub>4</sub> NO <sub>3</sub>	45	10,000	10,000	0.0

TABLE III

Separation of Pb(II) From the Solutions Containing Cu(II), Ni(II) Co(II)  
 Fe(II), Zn(II), Mn(II), Sr(II) and ZrO(II) in Ferric Phosphate (H-Form) Columns.

Separation	Eluents	Volume Effluent (ml)	Amount of Cation Loaded ( $\mu\text{C}$ )	Amount of Cation Recovered ( $\mu\text{C}$ )	Error %	$N^a$	$h^b$
Cu(II)-Pb(II)	Cu(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	35	5883	5851	-0.54	7.95	1.01
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		
Ni(II)-Pb(II)	Ni(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	20	2348	2348	0.0	10.20	1.01
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		
Zn(II)-Pb(II)	Zn(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	20	5393	5393	0.0	9.0	0.253
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		
Co(II)-Pb(II)	Co(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	25	4720	4777	+1.10	9.30	1.01
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		
Fe(II)-Pb(II)	Fe(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	25	10,932	10,932	0.0	86.0	1.01
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		
Mn(II)-Pb(II)	Mn(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	30	1705	1705	0.0	8.60	1.01
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		
Sr(II)-Pb(II)	Sr(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	25	4381	4381	0.0	8.30	1.01
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		
ZrO(II)-Pb(II)	ZrO(II)-0.01N-NH <sub>4</sub> NO <sub>3</sub>	25	2144	2144	0.0	8.60	1.01
	Pb(II)-0.1N-HNO <sub>3</sub> +1.0N-NH <sub>4</sub> NO <sub>3</sub>	50	7251	7251	0.0		

Note: a = liquor number of theoretical plates.

b = height equivalent to one theoretical plate.



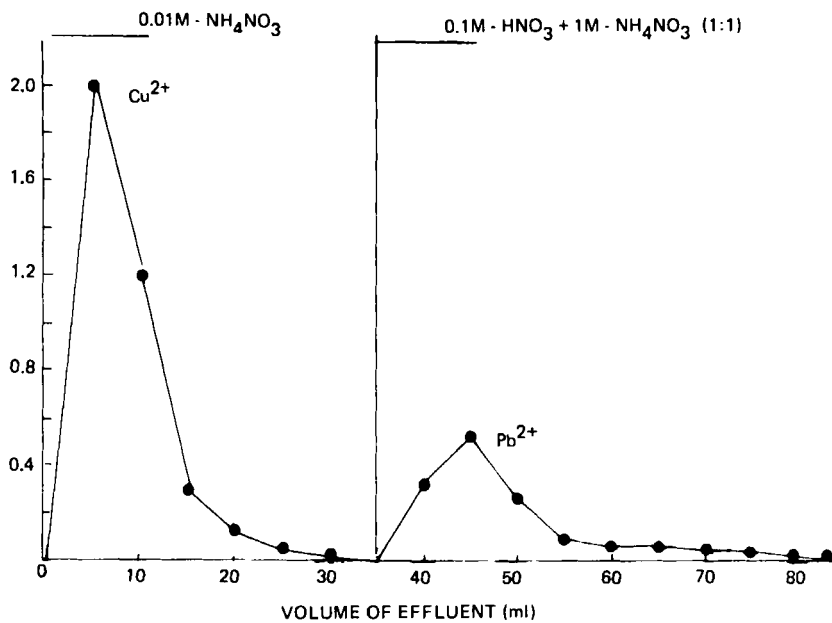


FIG. 1 SEPARATION OF Cu<sup>2+</sup> FROM Pb<sup>2+</sup>

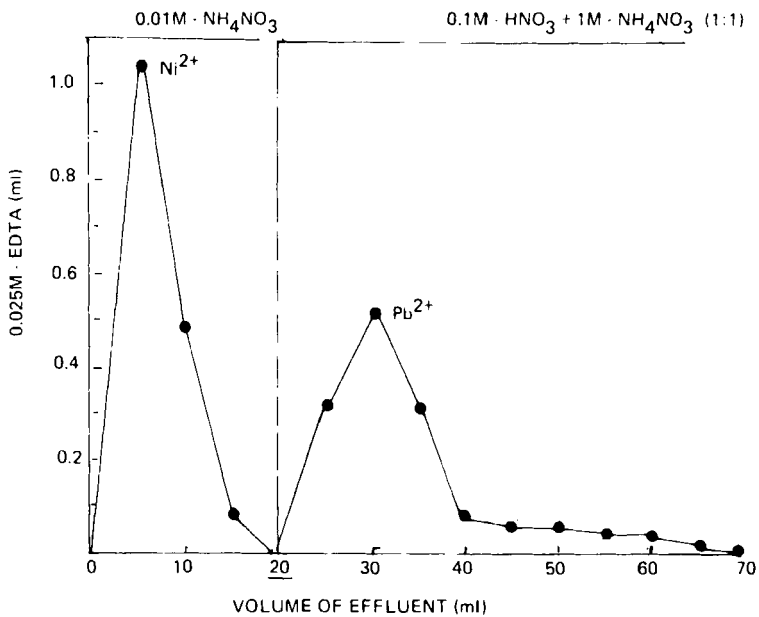


FIG. 2 SEPARATION OF Ni<sup>2+</sup> FROM Pb<sup>2+</sup>

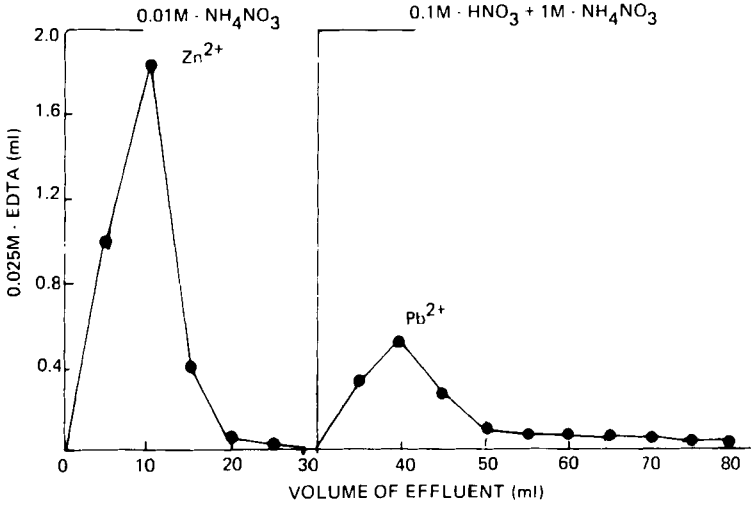


FIG. 3 SEPARATION OF Zn<sup>2+</sup> FROM Pb<sup>2+</sup>

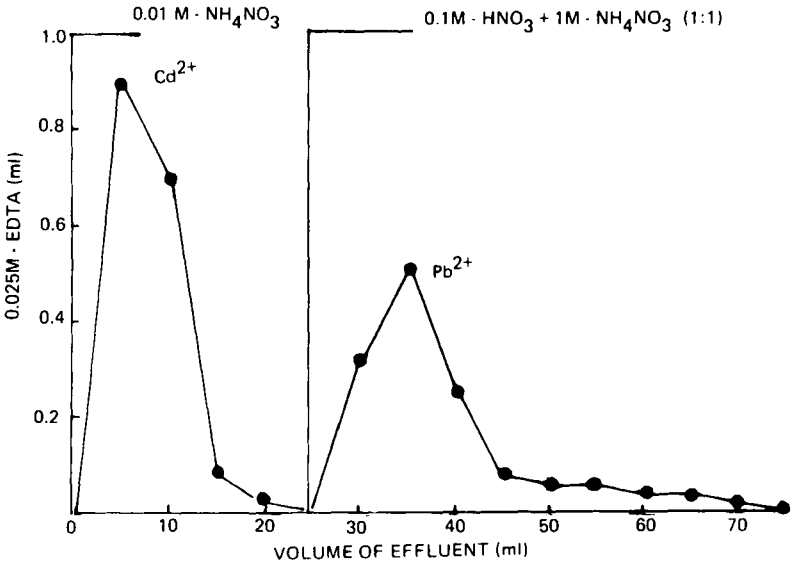


FIG. 4 SEPARATION OF Cd<sup>2+</sup> FROM Pb<sup>2+</sup>

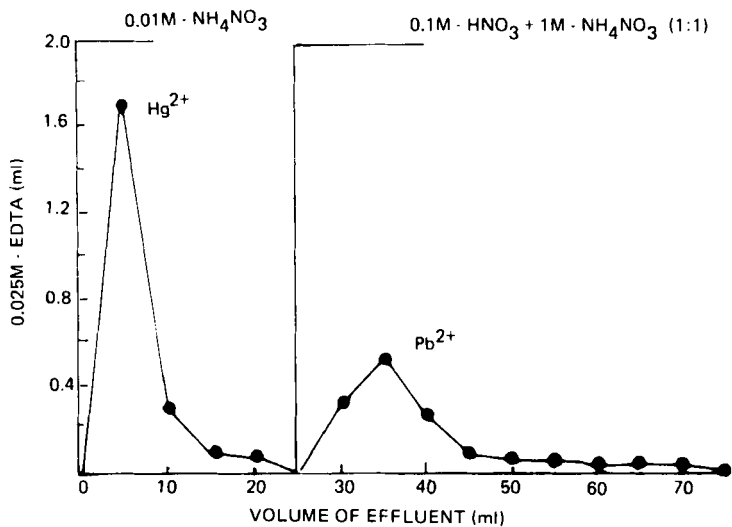


FIG. 5 SEPARATION OF Hg<sup>2+</sup> FROM Pb<sup>2+</sup>

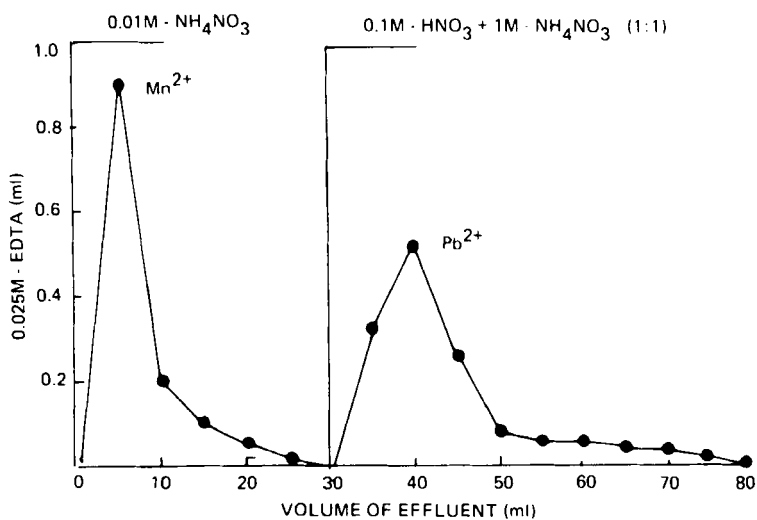


FIG. 6 SEPARATION OF Mn<sup>2+</sup> FROM Pb<sup>2+</sup>

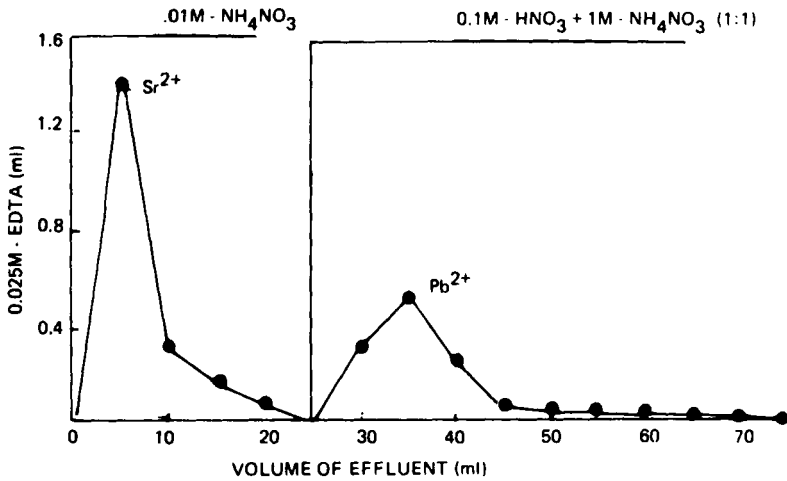


FIG. 7 SEPARATION OF  $Sr^{2+}$  FROM  $Pb^{2+}$

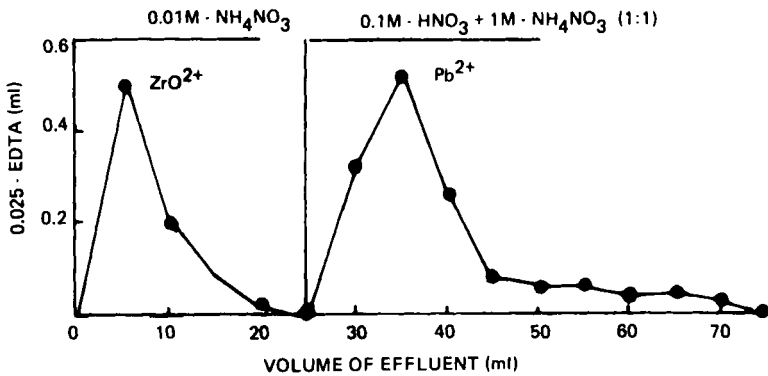


FIG. 8 SEPARATION OF  $ZrO^{2+}$  FROM  $Pb^{2+}$

and the other metal separated respectively.  $\epsilon$  is the Void fraction ( $\sim 0.4$ ). The values of height equivalent to one theoretical plate ( $h$ ) as reported in, TABLE-III, can be determined from the data obtained from an elution curve

$$h = \frac{L b^2}{8 v_{\max}^2}$$

where  $L$  is the length of the ion exchange column (cm),  $v_{\max}$  is the eluent volume at peak (ml) and  $b$  is the peak width (ml) at a height of  $0.368 C_{\max}$ .

#### Application to Pollution Studies:

The main sources of lead pollution are the industries manufacturing storage batteries, cable covering, paints and gasoline. Because Hg(II), Cu(II), Zn(II), Cd(II) and Ni(II) that react with dithizone are usually present in polluted samples. Hence, the proposed method of selective separation of Pb(II) followed by determination of lead by dithizone is the better method compared to other time consuming methods.

#### Application of Analysis of non-ferrous Alloys:

Lead is present as a major constituent of the following alloys: white metal bearing alloys, solders, type metals, leaded brasses and bronzes, various zinc-base die casting alloys and many others. The method of decomposition applied depends, of course, on the composition of the alloy to be analyzed. For this reason, no universally applicable procedure can be cited. Usually gravimetric methods are used for the analysis of alloys but these methods are time consuming. The proposed method is simple and rapid for the estimation of lead in various alloys as these alloys contain Cu, Ni, Cd, Zn, Mn as main constituents that can be selectively separated from Pb(II).

This method can also be used for the concentration of traces of lead in food products e.g. tea, coffee, sugar and butter. The final determination is made with dithizone spectrophotometrically.

#### ACKNOWLEDGEMENT

The authors are grateful to Prof. Harjit Singh for providing research facilities. One of us (H.S.) is also thankful to U.S.C. (India) for financial assistance.

REFERENCES

1. T.M.Florence and G.E.Batley, *Talanta* 24, 151 (1977).
2. I.M.Kelthoff and P.J.Elving, *Treatise on Analytical Chemistry*, vol.6 (II), 75 (1966).
3. J.P.Rawat and P.S.Thind, *Acta Ciencia India* 3(2), 120 (1977).
4. P.S.Thind and S.S.Sandhu, *J.Ind.Chem.Soc.*, LVI, 260 (1979).
5. P.S.Thind, *Annali Di Chimica* (Accepted for publication).
6. J.P.Rawat and P.S.Thind, *Can.J.Chem.*, 54, 192 (1976).